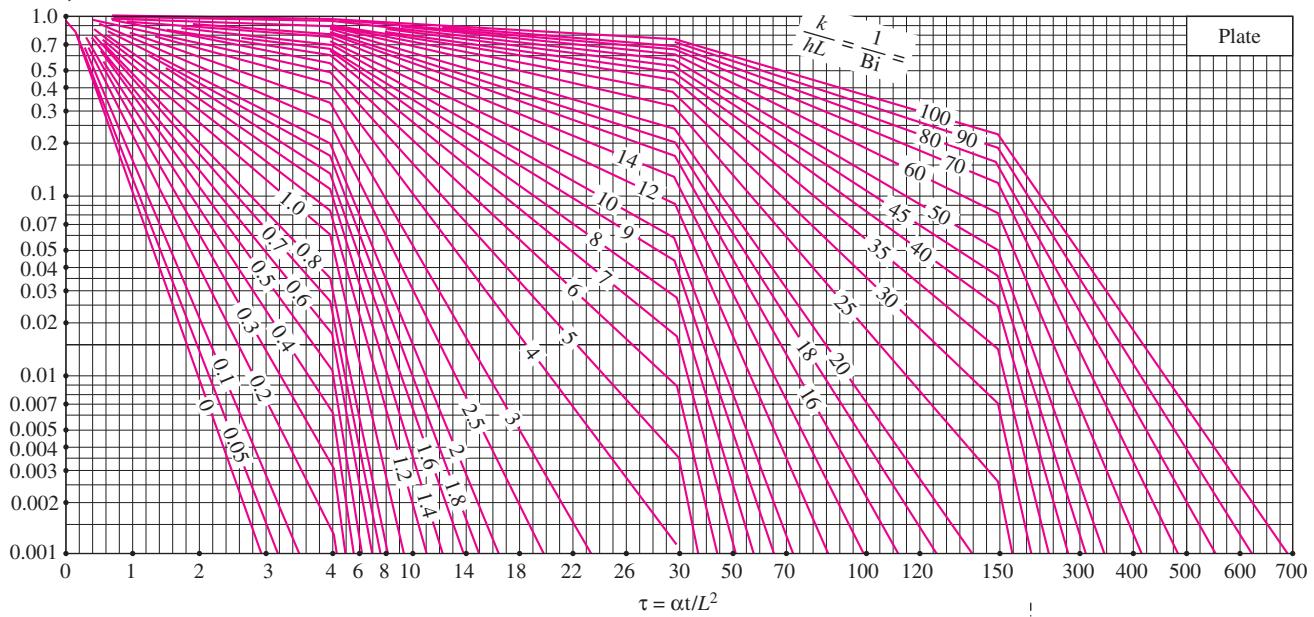
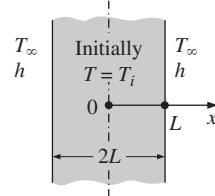


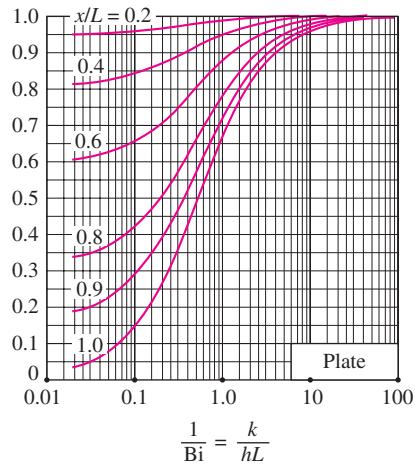
$$\theta_o = \frac{T_o - T_\infty}{T_i - T_\infty}$$



(a) Midplane temperature (from M. P. Heisler)

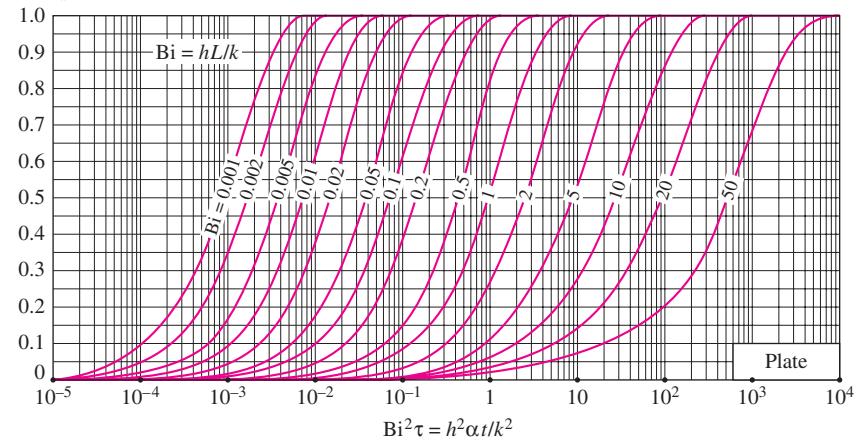


$$\theta = \frac{T - T_\infty}{T_o - T_\infty}$$



(b) Temperature distribution (from M. P. Heisler)

$$\frac{Q}{Q_{\max}}$$

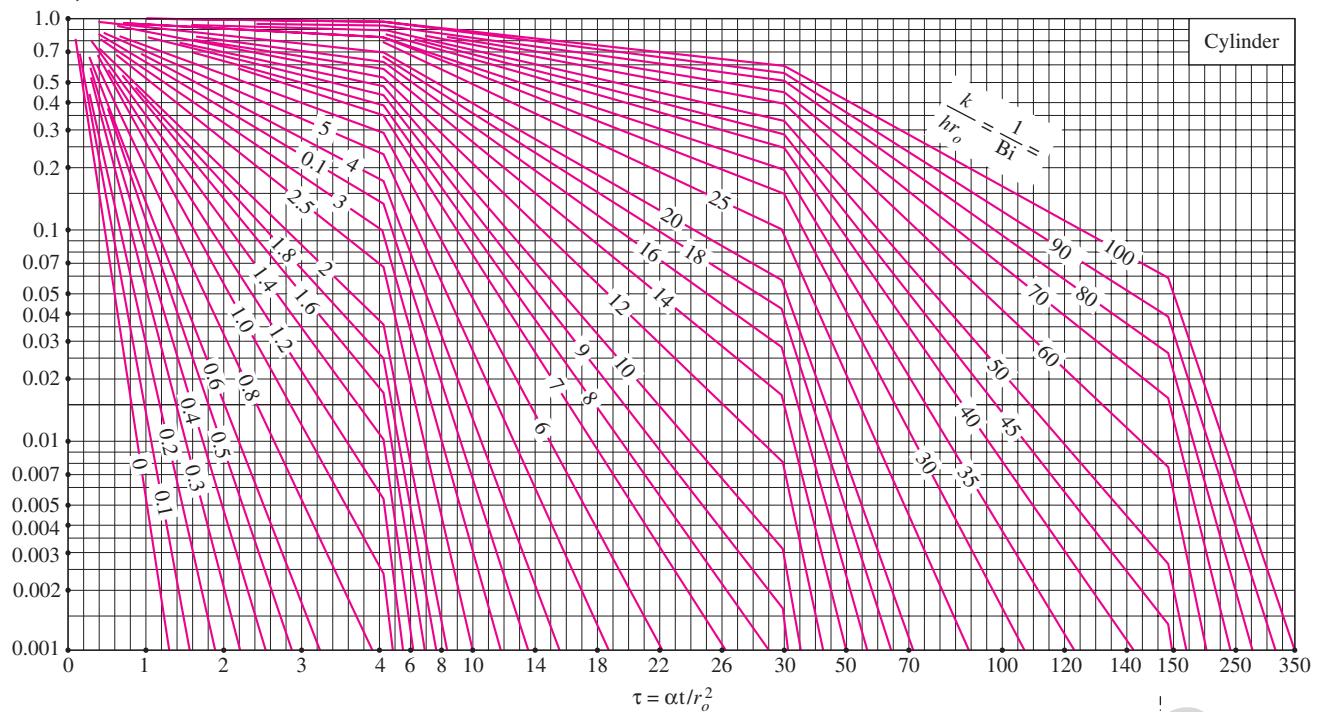


(c) Heat transfer (from H. Gröber et al.)

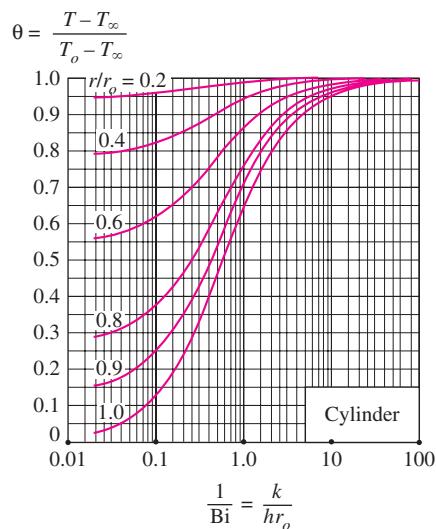
Transient temperature and heat transfer charts for a plane wall of thickness $2L$ initially at a uniform temperature T_i subjected to convection from both sides to an environment at temperature T_∞ with a convection coefficient of h .

where m is the mass, V is the volume, ρ is the density, and C_p is the specific heat of the body. Thus, Q_{\max} represents the amount of heat transfer for $t \rightarrow \infty$. The amount of heat transfer Q at a finite time t will obviously be less than this

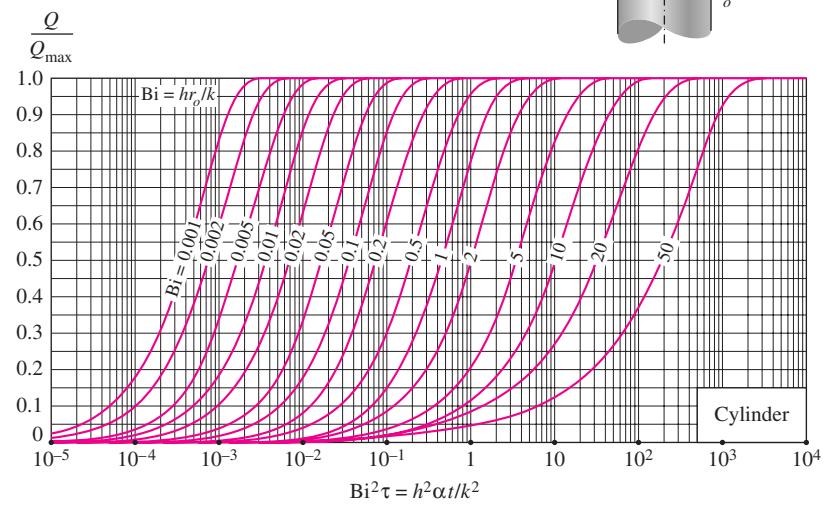
$$\theta_o = \frac{T_o - T_\infty}{T_i - T_\infty}$$



(a) Centerline temperature (from M. P. Heisler)



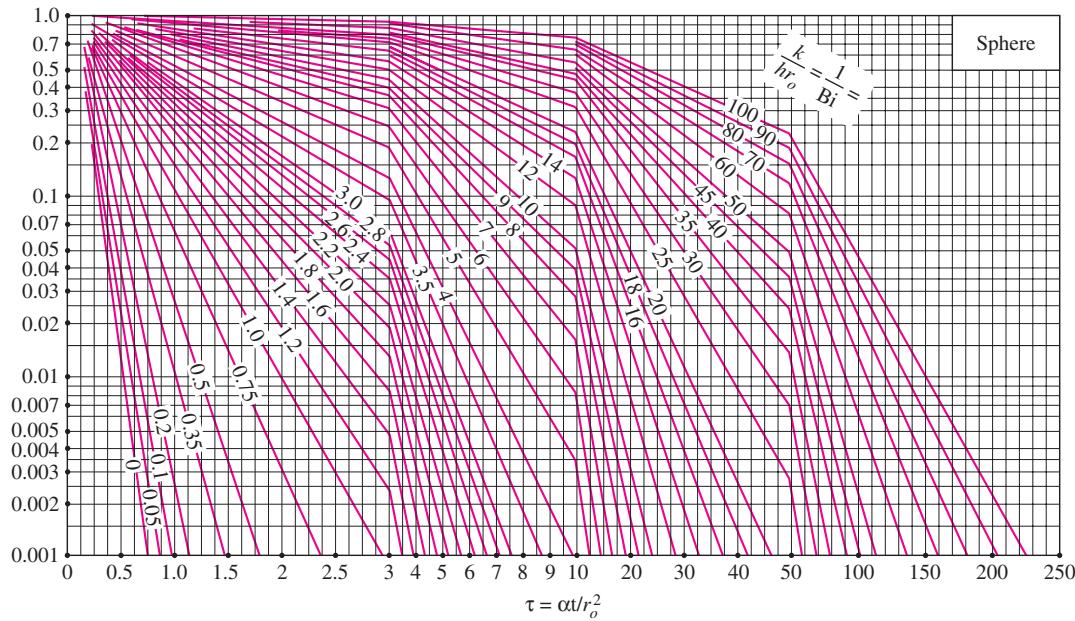
(b) Temperature distribution (from M. P. Heisler)



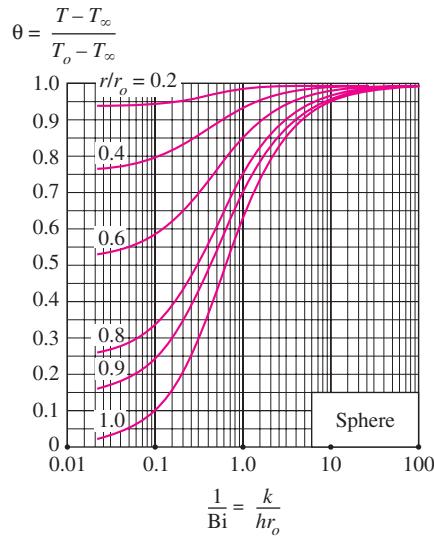
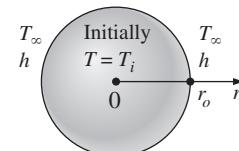
(c) Heat transfer (from H. Gröber et al.)

Transient temperature and heat transfer charts for a long cylinder of radius r_o initially at a uniform temperature T_i subjected to convection from all sides to an environment at temperature T_∞ with a convection coefficient of h .

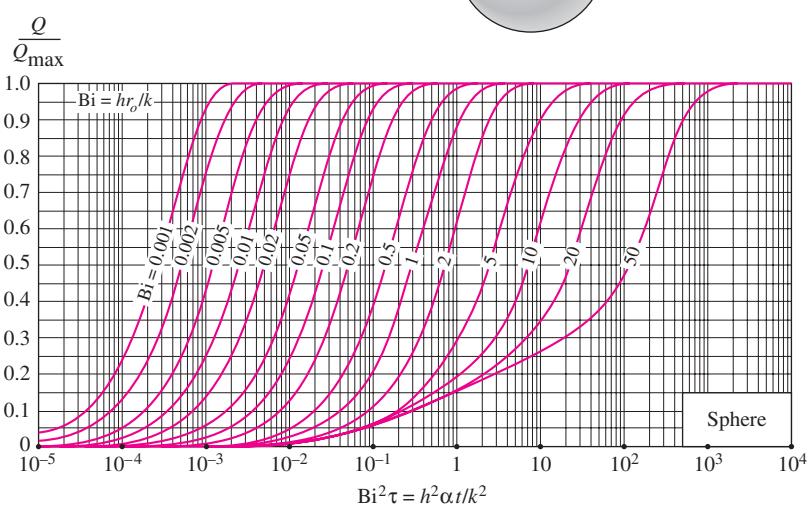
$$\theta_o = \frac{T_o - T_\infty}{T_i - T_\infty}$$



(a) Midpoint temperature (from M. P. Heisler)



(b) Temperature distribution (from M. P. Heisler)



(c) Heat transfer (from H. Gröber et al.)

Transient temperature and heat transfer charts for a sphere of radius r_o initially at a uniform temperature T_i subjected to convection from all sides to an environment at temperature T_∞ with a convection coefficient of h .

maximum. The ratio Q/Q_{\max} is plotted in Figures 4-13c, 4-14c, and 4-15c against the variables Bi and $h^2 \alpha t / k^2$ for the large plane wall, long cylinder, and